

Chapter 7

Heat transfer

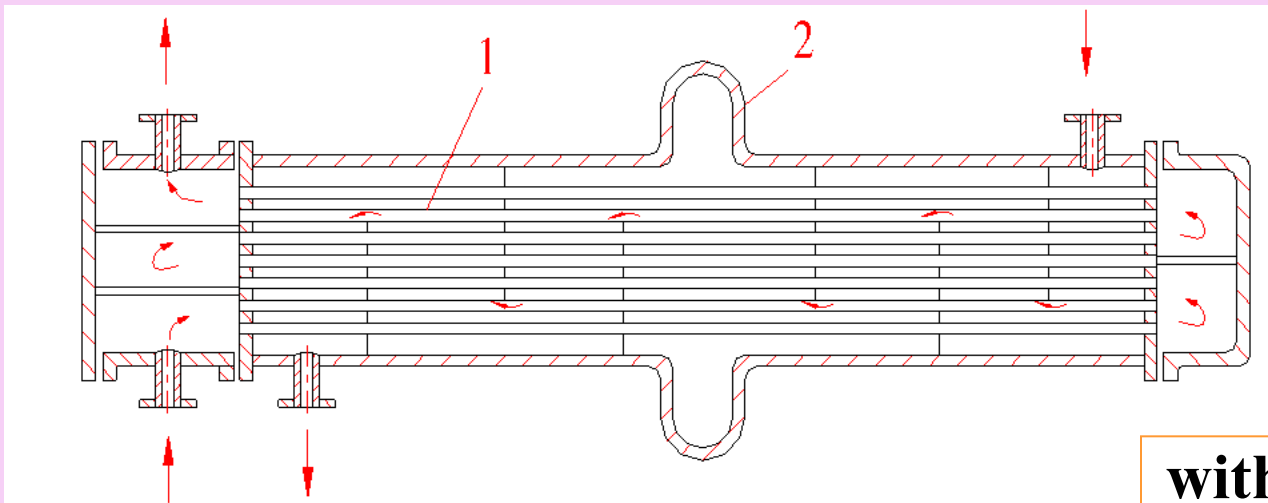
Evaluation of wall temperature

application

Calculating h (in condensation, boiling, natural convection and high viscosity situations)

Calculating heat loss, h_T

Considering heat compensation of exchanger



an heat exchanger
with four tube-pass
and one shell-pass

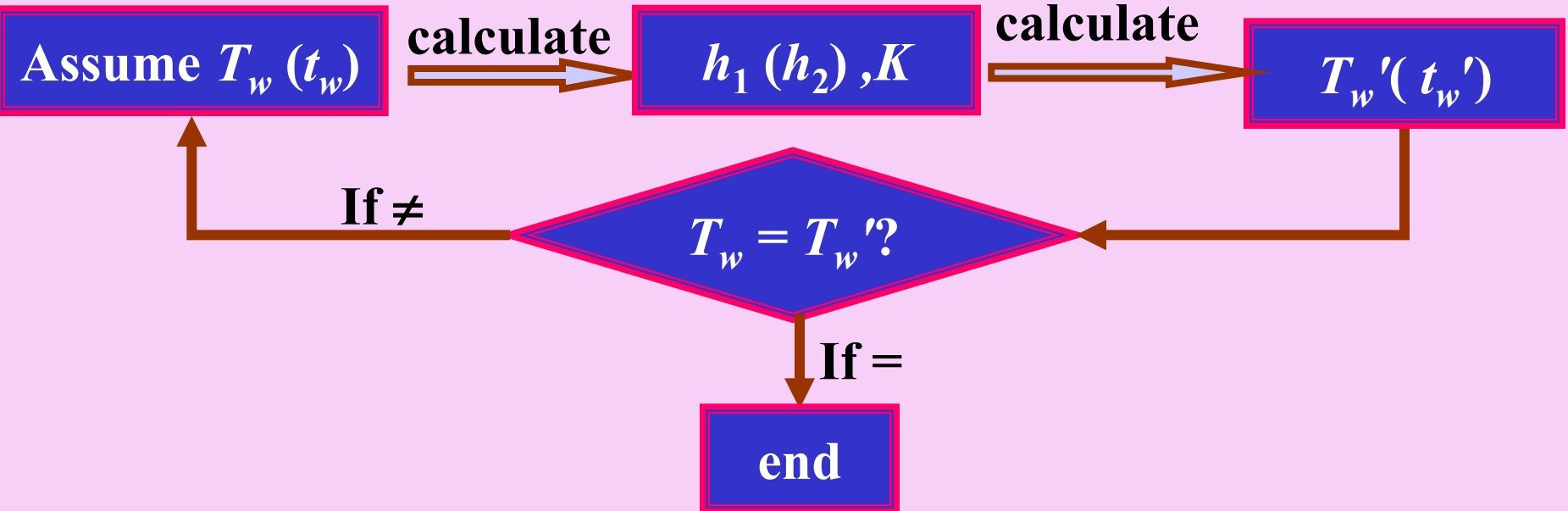
with expansion section

Helpful for selecting structure material

Ensuring product quality

Calculation by trial and error

$$Q = h_1 A_1 (T - T_w) = h_2 A_2 (t_w - t) = K_2 A_2 \Delta t_m$$



calculate h_1 (h_2) according to real situation

$$\frac{1}{K_2} = \frac{d_2}{h_1 d_1} + \frac{b}{k} \cdot \frac{d_2}{d_m} + \frac{1}{h_2}$$

$$T_w' = T - \frac{K_2 A_2 \Delta t_m}{h_1 A_1} \quad \text{or} \quad t_w' = t + \frac{K_2 \Delta t_m}{h_2}$$

Brief evaluation

$$T_w \approx t_w = \frac{h_1 T_m + h_2 t_m}{h_1 + h_2}$$

where $T_m = (T_1 + T_2)/2$, $t_m = (t_1 + t_2)/2$

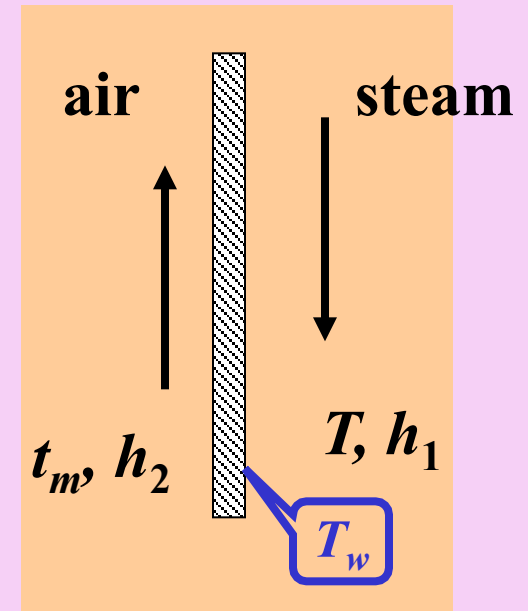
tendency of wall temperature

If $h_1 \gg h_2$, let $A_1 \approx A_2$, $t_w \approx T_w$

From

$$Q = \frac{T - T_w}{\frac{1}{h_1}} = \frac{T_w - t_m}{\frac{1}{h_2}}$$

For a certain Q , if $1/h_1$ is small, then $T - T_w$ is also small, T closes to T_w ; if $1/h_2$ is large, then $T_w - t$ is large and, t is quite different with T_w .



Wall temperature is close to the fluid temperature with large h .

7.7 Enhance and weaken of heat transfer

enhance

$$Q = K A \Delta t_m = \frac{\Delta t_m}{\frac{1}{K A}}$$

$$K \uparrow, A \uparrow, \Delta t_m \uparrow, R \downarrow; Q \uparrow$$

a. Increasing A —not by large equipment size, but by improving the structure to increase area per unit volume.

- tube with fins on surface
- tube with screw surface
- tube of small diameter when $D < 1000\text{mm}$, if diameter $\phi 25 \rightarrow \phi 19$, the total A will increase more than 35%.



- Coating or sintering small metal particles on the heating surface will give large area. Useful for boiling heat transfer.

Enhancement

b. Increasing K

$$\frac{1}{K_2} = \frac{d_2}{h_1 d_1} + R_{s1} + \frac{b}{k} \cdot \frac{d_2}{d_m} + R_{s2} + \frac{1}{h_2}$$

- * **increase fluid velocity** — especially for reducing key resistance
- * **changing flow pattern** —increase turbulence to reduce the thickness of laminar sub-layer.
- * **adding solid particles** —to increase turbulence and erase scaling.
- * **removing scaling** regularly and in time

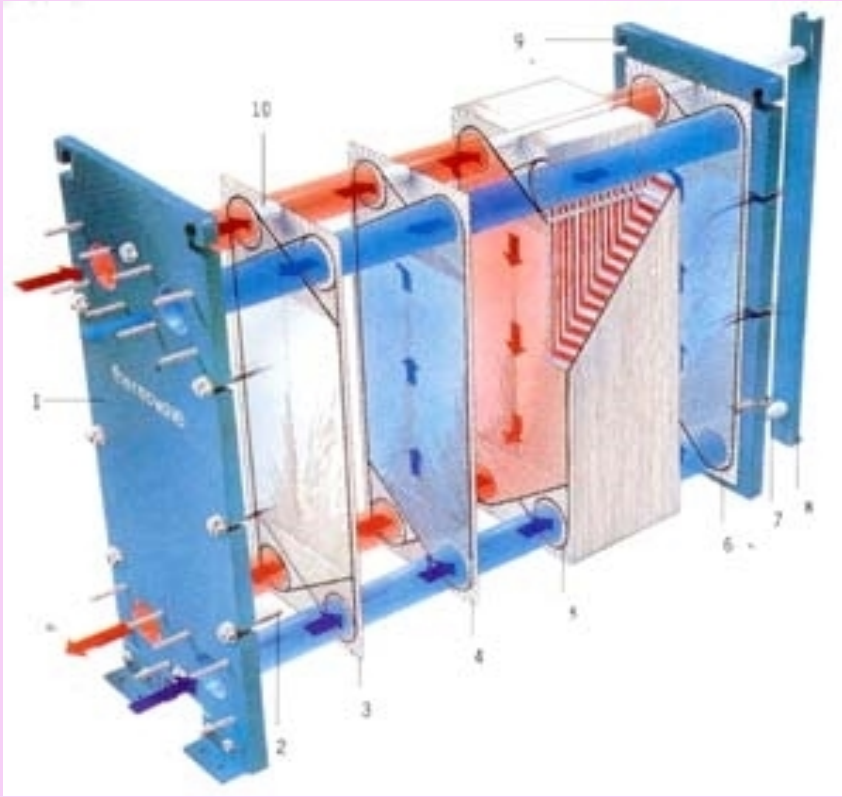
c. Increasing Δt_m — use counter current

weaken of heat transfer

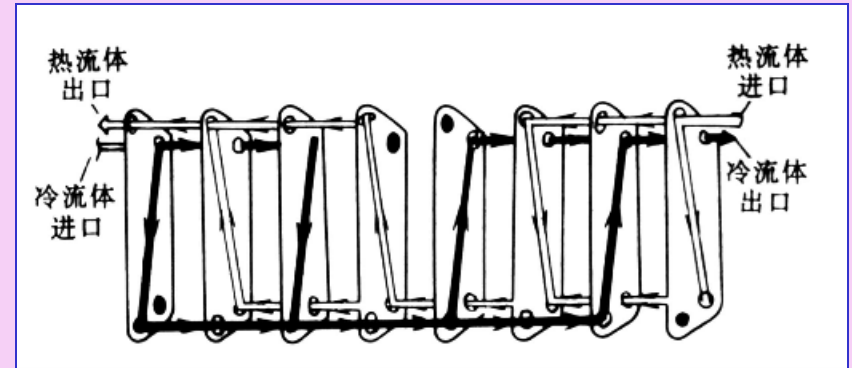
——heat isolation and reflection technology

Heat exchangers

Flat plate heat exchanger



- 1.固定压紧板
- 2.夹紧螺栓
- 3.前端板
- 4.换热板片
- 5.密封垫片
- 6.后端板
- 7.下导板
- 8.后支柱
- 9.活动压紧板
- 10.上导板





Flat plate heat exchanger

Advantages

- **compact structure** For same heat transfer area, the size and weight is about $1/3 \sim 1/5$ of pipe-shell exchangers.
- **high h** When $Re > 10$, strong turbulent flow, K can achieve $3000 \sim 8000 \text{ W/m}^2 \cdot \text{K}$.
- **small end temperature difference** about 1°C because of the countercurrent.
- **small heat loss** Heat efficiency $\geq 98\%$, heat isolation may not be needed.
- **easily adjustment**
- **low fluid retaining**
- **low scaling and block tendencies**
- **Low equipment cost** because of light weight

Disadvantages

- * **low flow rate because of its structure**
- * **low operation pressure usually < 2 MPa**
- * **low temperature because of the gasket material.**
Usually lower than 250°C .



以上内容仅为本文档的试下载部分，为可阅读页数的一半内容。如要下载或阅读全文，请访问：<https://d.book118.com/998022127005006113>